



Potential of aquacultural sludge treatment for aquaponics: evaluation of nutrient mobilization under aerobic and anaerobic conditions

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ABSTRACT: In recirculating aquaculture systems (RAS), mechanical removal of suspended solids by clarifiers or drum filters provides an organic mixture rich in nutrients. Still, in most traditional RAS, this sludge is discharged directly or following dewatering. Here, the potential recycling of nutrients from sludge is assessed, comparing aerobic and anaerobic mobilization of nutrients experimentally, ultimately aiming at an application in aquaponic systems. Nutrient mobilization processes were studied, monitoring soluble nutrients photometrically in the treatment tanks (NO_3^- -N, NO_2^- -N, total ammonia nitrogen, soluble reactive phosphorus [SRP], K^+ , Mg^{2+} and Fe^{2+}), the nutrient composition of the sludge (total phosphorus, Fe, Mn, Al, S, Mg, Ca) by inductively coupled plasma optical emission spectrometry, as well as C:N ratio, total solids (TS) and total suspended solids (TSS). Aerobic treatment (aerated, AT) resulted in a 3.2-fold increase in mean (\pm SD) SRP from 9.4 (\pm 0.7) to 29.7 (\pm 2.1) mg l^{-1} , most likely owing to a decrease in pH. In contrast, in the anaerobic treatment (unaerated, UT), SRP remained unchanged between 9.4 (\pm 0.7) and 9.3 (\pm 0.4) mg l^{-1} . Both treatments resulted in increased K^+ concentrations from 28.1 (\pm 1.5) to 36.8 (\pm 2.3) mg l^{-1} in AT and to 32.2 (\pm 2.3) mg l^{-1} in UT. AT revealed best mobilization of P and K^+ without major losses of NO_3^- -N. Thus, aerobic treatment of water-sludge mixture has a high potential for significant improvements of nutrient recycling in aquaponics.

KEY WORDS: Aquaponics · Phosphate recovery · Nitrate · Sludge · Aerobic · Anaerobic · Nutrient recycling

INTRODUCTION

Public perception of aquaculture is often critical, raising concerns about eutrophication and pollution of the aquatic environment due to direct emissions of nutrients from fish farms (Edwards 2015, Zhang et al. 2015). Often ignored, solid waste originating from faeces and uneaten feed pellets represent a substantial nutrient reservoir. Upon microbial conversion, chemical mobilization and leaching, nutrient emissions may induce algal blooms, oxygen depletion and mass mortalities among aquatic or-

ganisms (Zhang et al. 2015). Over the last 2 decades, recirculating aquaculture systems (RAS) have been rapidly evolving to reduce such impacts on the environment. Undoubtedly, RAS technology has a great potential, particularly assigned to the efficient use of water and space (Gutierrez-Wing & Malone 2006) and supports a sustainable development of the fast growing aquaculture industry. Environmental legislation and, from an economic perspective, fees for waste disposal and nutrient emissions represent main motivations to improve waste management and reduce nutrient emission supporting the

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development of sound environmentally friendly aquaculture production.

RAS usually comprise 2 main water treatment steps. First, mechanical filters such as clarifiers or drum filters are used to concentrate suspended solids, discharged either after dewatering or directly with the backwash. Subsequently in a biofilter, toxic ammonia, ($\text{NH}_4^+/\text{NH}_3$) excreted from the fish gills, is converted to nitrate (NO_3^-) by nitrifying bacteria (Paredes et al. 2007). Despite the large variability observed between species, 60–90% of the excreted nitrogen is dissolved (van Rijn 2013). In contrast to classical RAS, aquaponic systems make use of such soluble nutrients derived from the fish unit to grow plants in an integrated hydroponic unit (Goddek et al. 2015). Here, standing stock of the RAS sustains the growth of the crop plants hence determining the dimensions of the hydroponic production (Rakocy et al. 2006). Consequently, in a well-balanced system, additional nitrogen fertilization is not required.

In contrast, phosphorus (P) in the process water is generally limited, but is essential for plant growth (Dawson & Hilton 2011) and can only be assimilated by plants as dissolved inorganic phosphate (PO_4^{3-} ; hereafter soluble reactive phosphorus, SRP). A high percentage of the dietary P is not retained in fish but excreted and dissolved P strongly adsorbs onto particles (Neori et al. 2007). Consequently, feed leftovers and fish faeces are the main sources for P, either in organic form or inorganic as PO_4^{3-} (Barak & van Rijn 2000). Thus, mechanical removal of suspended solids removes a major part of P without considering further strategies for recycling. Recent fishmeal substitution in modern diets reduces SRP (Hua & Bureau 2006) but further increases the deposition of plant-derived organic phosphorus in the sludge.

In addition to P, the supply of potassium (K^+) is often suboptimal in aquaponic systems (Rakocy et al. 2006). Consequently, it has become standard practice in aquaponics to use synthetic chemical fertilizers, mainly nitrogen, phosphate and potassium (NPK-fertilizer) to formulate aquaponic media if specific nutrient profiles are not met (Rennert et al. 2011).

To date, the management of aquacultural sludge mostly aimed for improved water recycling in RAS as well as in aquaponics. Obviously, optimization strategies in RAS and aquaponics are quite opposite. In RAS, efforts focus on higher nutrient retention in the fish or the use of sludge as a nutrient sink. In aquaponics, retention of nutrients in the fish is not necessarily prioritized. Instead, optimized mobiliza-

tion of nutrients is a key factor to ensure sustainability of the system. Currently, the prevailing approach used in RAS is anaerobic sludge digestion to reduce organic matter (Mirzoyan et al. 2010, Jung & Lovitt 2011). Here, to mobilize P, manipulation of pH is often carried out, either by addition of acids or indirectly via microbial fermentation (Jung & Lovitt 2011). Only very few studies considered aerobic treatment for nutrient recycling of sludge where inorganic P is mobilised from organic P compounds by microbial dephosphorylation (Rakocy et al. 2007, Neori et al. 2007). Still, high mobilization rates of nutrients under aerobic conditions have been documented (Neori et al. 2007, Rakocy et al. 2007). Furthermore, under aerobic conditions, excessive nitrogen loss due to denitrification is prevented. Here, relevance of nitrogen recycling remains to be evaluated in a comparative approach under realistic production conditions, as a major part of nitrogen is actually soluble. More importantly, realistic data of P and K mobilization is needed to improve nutrient management in aquaponics.

In this study, we investigated the potential utilization of aquaculture sludge (i.e. solid waste collected in the mechanical treatment unit such as clarifier or drum filter) comparatively assessing nutrient mobilization under aerobic and anaerobic conditions. This study was integrated in a 6 mo trial on the optimization of a coupled and a decoupled aquaponic system (H. Monsees et al. unpubl.).

Optimizing sludge management should ultimately provide sound data to (1) improve environmental sustainability in the context of nutrient recycling and reduced emissions as well as profitability (reduced costs due to high water recovery from the sludge, decreased fertilization and, most importantly, lower waste and emission fees) and (2) increase the self-reliance of aquaponics. Finally, this will support the development of an automated or semi-automated reactor which will allow continuous, optimized nutrient mobilization to support a closed nutrient loop in aquaponics irrespective of the mechanical filter used (e.g. drum filter, clarifier).

MATERIALS AND METHODS

Aquaponic system

Experiments were conducted at the aquaponic research facility of the Leibniz-Institute of Freshwater Ecology and Inland Fisheries (IGB, Berlin, Germany), using a RAS with a total water volume of

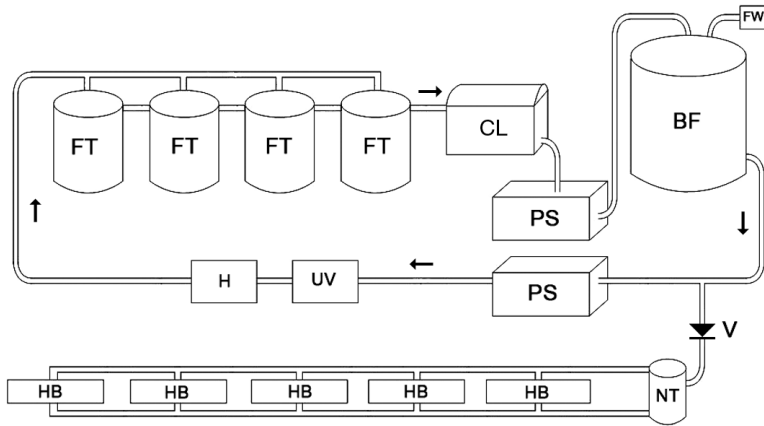


Fig. 1. Coupled aquaponic system, comprising a recirculating aquaculture system and a hydroponic unit. FT: fish tank(tanks are set up in parallel, with each outflow draining to the clarifier via an open channel behind the tanks); CL: clarifier; PS: pump sump; BF: biofilter; FW: fresh water supply; UV: UV disinfection unit (optional); H: heater (optional); HB: hydroponic beds (nutrient flow technique); NT: nutrient media reservoir; V: 1-way valve

16.5 m³ (Fig. 1). Three separate rearing tanks (1.7 m³ each) were stocked with a total of 316 kg tilapia *Oreochromis niloticus* L. at rearing densities of 62 kg m⁻³ per tank.

Fish originated from a brood stock established at the IGB and were not further characterized. Removal of suspended matter was carried out with a clarifier (1.5 m³). Over the experimental period, fish were fed a commercial diet at 0.8% of their body weight per day (Aller Float 37/10 2 mm, Emsland-Aller Aqua: 37% protein, 10% fat, 38.5% nitrogen-free extract, 6% ash, 3% fibre, 1.2% P of dry weight; estimated environmental impact (feed conversion ratio = 1.0): 4.7 g N and 3 g P in faeces per kg feed, 27 g N and 2.7 g P in water per kg feed).

Temperature, pH and oxygen were determined daily (HQ40d multi, Hach Lange); pH was regulated with Ca(OH)₂ to maintain a target pH of 7 (±1) (Table 1). Selected nutrients (NO₃⁻-N, cadmium reduction method #8039; NO₂⁻-N, USEPA diazotization method #8507; total ammonia nitrogen [TAN], salicylate

Table 1. Rearing conditions for tilapia during the experimental period

Parameter	Target value
Temperature (°C)	26 ± 1
Oxygen (mg l ⁻¹)	>5
pH	7 ± 1
Stocking density (kg m ⁻³)	62 ± 2.5
Feeding rate (%)	0.8
Feed (kg d ⁻¹)	2.5

method #8155; K⁺, tetraphenylborate method #8049; Mg²⁺, calmagite colorimetric method #8030; Fe²⁺, 1,10-phenanthroline method #8146; all methods from the manufacturer's manual; Hach Lange) in the water were determined spectrophotometrically (DR3900, Hach Lange) at the inlet of a fish tank and the outlet of the clarifier (see Table 4). SRP (see Figs. 2a & 3a) was measured photometrically (Spekol® 1500, Analytik Jena) at a wavelength of 880 nm according to the molybdenum blue method (Murphy & Riley 1962). Conditions in the RAS are summarized in Table 1. The water-sludge mixture (1.5 m³) from the clarifier was collected once weekly in a 2 m³ tank, homogenized with a pump and used for the subsequent experiments.

Determination of total suspended solids (TSS) in the RAS

For TSS, water samples (620 ml) were taken in triplicate at the inflow of a fish tank prior to feeding at 09:00 h (0 h), and 3, 6, 9 and 24 h thereafter. Briefly, samples were filtered through pre-weighed 0.45 µm CA membrane filters (GE Healthcare), freeze-dried to constant weight and weighed.

Sludge composition

Total solids (TS) were determined in a subsample of the homogenized water-sludge mix after centrifugation and freeze-drying to constant weight. Total phosphorus (TP), iron (Fe), manganese (Mn), aluminum (Al), sulfur (S), magnesium (Mg) and calcium (Ca) were determined by inductively coupled plasma optical emission spectrometry (iCAB 6000, Thermo Fisher Scientific) after wet digestion (HCl 37%, HNO₃ 65%, volumetric ratio 1:3) in a high pressure microwave oven (Gigatherm). C:N analysis was performed using freeze-dried, weighed sediment packed in tin foil and analyzed in a Vario EL© system (Elementar Analysensysteme). Dry weight: wet weight ratio was determined in freeze-dried aliquots of fresh sludge (n = 15).

Expt 1: Anaerobic lab-scale nutrient mobilization

For the verification of nutrient mobilization under anaerobic conditions in a closed container, lab-scale

experiments were performed. The water-sludge mix was transferred to 18 centrifugation tubes (55 ml), ensuring that no air remained inside the tubes. To minimize temperature variation, tubes were incubated on a rotation shaker (Heidolph Reax) in a climate chamber at $25 \pm 0.5^\circ\text{C}$ for 4 d (with an additional 4 d for SRP sampling only). Each day, 3 tubes were sampled for nutrient determination (SRP, NO_3^- -N, NO_2^- -N, TAN, K^+ , Mg^{2+} and Fe^{2+}). Briefly, samples were centrifuged (Multifuge 1-sr, Thermo Fisher) for 10 min at $1900 \times g$. Directly before analysis, the liquid phase was filtered through a $0.45 \mu\text{m}$ nylon syringe filter (Braun). According to O'Sullivan & Reynolds (2004), dissolved $\text{O}_2 < 0.1 \text{ mg l}^{-1}$ is considered anaerobic here. To exclude oxygenation of the small volume during measurement, oxygen was determined separately, using 500 ml glass bottles ($n = 3$) filled completely with water-sludge mix and continuously monitored with an oxygen probe inserted through a parafilm seal. Additionally bottles were covered with aluminium foil to prevent algal growth and placed on a magnetic stirrer (Heidolph MR 1000) for continuous movement of the liquid. Oxygen concentration was measured at 5 min intervals.

Expt 2: Aerated (aerobic) and unaerated (anaerobic) nutrient mobilization

Homogenized water-sludge mix was distributed to six 30 l polyethylene tanks providing an aerated (compressed air via airstones), aerobic (AT) and an unaerated, anaerobic treatment (UT), assessed in 3 replicates each over 14 d and repeated 3 times. All boxes were covered with a tight lid to prevent evaporation and incubated in a water bath ($1.5 \times 1.5 \text{ m}$ glass fibre tank equipped with two 300 W heaters and a pump for constant circulation) at $26^\circ\text{C} \pm 0.6^\circ\text{C}$ for the 14 d. The water bath was additionally insulated with foil and covered with thick, black pond foil

to prevent algal growth. Samples for water analysis were collected in 50 ml centrifugation tubes and directly analyzed for dissolved ions as described for Expt 1.

Statistical analysis

Data are presented as means \pm standard deviation (SD) of n samples. Statistical analysis was performed using Graphpad Prism (GraphPad Software). Data were tested for normality (Shapiro-Wilk) and equal variance (Kruskal-Wallis). Multiple comparison was carried out by non-parametric Dunn's test ($p < 0.05$), and pairwise comparisons were carried out by non-parametric Mann-Whitney U test ($p < 0.05$).

RESULTS

Characterization of the sludge-water mixture

Sludge collected successively from a full production cycle for tilapia under realistic conditions was comparable between all 4 replicates with regard to element composition (Table 2). Only slight variations ($<20\%$) were observed, particularly P, Ca, and most prominently in TS. A mean P deposition of 59.4 g wk^{-1} was observed in the clarifier. TSS was highest in the morning (Table 3), but decreased within 3 h, fluctuating around 1.5 mg l^{-1} (± 0.2).

The soluble nutrients measured at the outlet of the clarifier and at the inlet of the fish tanks were comparable (Table 4). As expected, TAN and NO_2^- -N in the rearing water of the RAS were always below critical threshold. NO_3^- -N concentration varied, providing different starting points for the experiments (highest concentration during the first sampling of Expt 2). Phosphate, magnesium and potassium also varied slightly, but not strictly correlated to each other.

Table 2. Elemental analysis by inductively coupled plasma optical emission spectrometry, C:N ratio and total solids (TS) of freeze-dried sludge collected from the clarifier (1.5 m^3) of a recirculating aquaculture system producing tilapia under realistic conditions in 4 technical replicates, illustrating the respective variation in sludge harvested during the experimental period

Replicate	P (mg g^{-1})	Mg (mg g^{-1})	Ca (mg g^{-1})	Fe (mg g^{-1})	Mn (mg g^{-1})	Al (mg g^{-1})	S (mg g^{-1})	C (%)	N (%)	C:N	TS (g l^{-1})
1	31.27	3.32	56.35	3.69	0.27	3.31	6.75	35.59	3.87	9.18	1.23 ± 0.05
2	25.46	3.30	47.77	2.84	0.23	2.22	6.04	37.61	4.08	9.21	1.14 ± 0.04
3	28.84	3.25	50.51	2.95	0.21	2.69	5.86	36.54	4.00	9.15	1.65 ± 0.03
4	35.92	3.22	70.01	3.38	0.27	3.18	7.53	33.95	4.43	7.67	–

Table 3. Total suspended solids (TSS, g dry weight l⁻¹ rearing water) in a tilapia recirculating aquaculture system over 24 h. Samples were taken at the inlet of a fish tank; sampling started at 09:00 h before feeding. Data are means \pm SD (n = 3)

Time (h)	TSS (mg l ⁻¹)
0	2.3 \pm 0.1
3	1.5 \pm 0.1
6	1.6 \pm 0.3
9	1.4 \pm 0.3
24	2.2 \pm 0.2

Expt 1: Anaerobic lab-scale mobilization

Within 8 d, SRP increased steadily in all 3 successively assessed sludge-water mixtures. At 0 d, SRP ranged between 7.8 and 9.2 mg l⁻¹ and increased significantly ($p < 0.05$, Dunn's) to 11.2–12.6 mg l⁻¹ (Fig. 2a). Only minor oscillations were observed in K⁺, revealing concentrations of approximately 25.0 mg l⁻¹ (Fig. 2b). The NO₃⁻-N concentration was reduced by 97% within 4 d from 58 (\pm 8) to 1.5 (\pm 0.2) mg l⁻¹ (Fig. 2c). In parallel, TAN increased substantially ($p < 0.05$, Dunn's) from <1 mg l⁻¹ to >10 mg l⁻¹ (Fig. 2d). NO₂⁻-N concentrations decreased significantly ($p < 0.05$, Dunn's) from 1.4 (\pm 0.4) to 0.03 (\pm 0.03) mg l⁻¹ (Fig. 2e). Mg²⁺ did not vary over the 4 d (64.1 \pm 1.2 mg l⁻¹; Fig. 2f). Fe²⁺ concentrations were always below the detection limit (<0.01 mg l⁻¹; data not shown). Measurement of oxygen concentration in sealed glass bottles (see 'Materials and methods') revealed a complete depletion of oxygen from 5.28 to 0 mg l⁻¹ within 45 min (data not shown), confirming anaerobic conditions.

Expt 2: Aerobic and anaerobic mobilization

Within 14 d (Day 0 to Day 13), SRP increased significantly ($p < 0.05$, Mann-Whitney) in the AT from 9.4

Table 4. Soluble nutrients (PO₄³⁻, K⁺, total ammonia nitrogen [TAN], NO₃⁻-N, NO₂⁻-N, Mg²⁺) measured at the inlet of a fish tank and the outlet of the clarifier of a tilapia recirculating aquaculture system. Data are the results of 3 successive samplings. nd: parameters not determined

Parameter (mg l ⁻¹)	Sampling 1		Sampling 2		Sampling 3	
	Tank	Clarifier	Tank	Clarifier	Tank	Clarifier
TAN	0.3	0.2	0.2	0.4	0.2	0.4
NO ₂ ⁻ -N	0.1	0.2	0.1	0.1	nd	nd
NO ₃ ⁻ -N	64.0	63.0	48.5	50.0	46.5	52.5
PO ₄ ³⁻	7.9	8.0	8.1	7.9	9.7	9.5
Mg ²⁺	61.6	63.0	59.2	62.6	70.0	70.4
K ⁺	27.0	26.5	24.5	24.5	28.5	27.0

(\pm 0.8) to 29.7 (\pm 2.1) mg l⁻¹ PO₄³⁻ (Fig. 3a). In contrast, no changes were observed in the UT. In the AT, K⁺ concentration increased by 30% from 28.1 (\pm 1.5) to 36.8 (\pm 2.3) mg l⁻¹ between 0 d and 14 d (Fig. 3b). Again, NO₃⁻-N dropped from 68.2 (\pm 2.8) to 9.4 (\pm 4.4) mg l⁻¹ in the UT and was thus reduced by 86% within 14 d (Fig. 3c); in contrast, only a minor reduction of 16% from 68.2 (\pm 2.8) to 55.1 (\pm 11.3) mg l⁻¹ was observed in the AT (Fig. 3c). In the UT, TAN increased from 1.0 (\pm 0.1) to 7.9 (\pm 0.8) mg l⁻¹, but decreased from 1.0 (\pm 0.1) to 0.1 (\pm 0.1) mg l⁻¹ in the AT (Fig. 3d). Initially, NO₂⁻-N decreased in both treatments, but from Day 7 in the UT it then increased to 0.2 (\pm 0.1) mg l⁻¹ (Fig. 3e). In the AT, NO₂⁻-N dropped continuously from 1.3 (\pm 0.4) to 0.01 (\pm 0.005) mg l⁻¹. No changes in Mg²⁺ were observed over time, neither between treatments nor within a treatment (AT: 61–73 mg l⁻¹; UT: 53–74 mg l⁻¹; Fig. 3f). In both treatments, iron concentrations were always below the detection limit (Fe²⁺ \leq 0.01 mg l⁻¹; data not shown).

AT and UT revealed opposite progression in pH, increasing from 6.2 (\pm 0.02) to 7.0 (\pm 0.2) in the UT and decreasing to 5.3 (\pm 0.01) in the AT (Fig. 4).

DISCUSSION

Here, sludge obtained from the clarifier of a RAS was used to demonstrate the potential of optimized nutrient mobilization for aquaponics, aiming at an easy-to-handle, inexpensive/economical incubator. Aeration treatment (AT) increased the P concentration by 330% and the K⁺ concentration by 31% within 14 d of incubation. This is highly relevant since most K⁺ and P input via the feed is actually retained in the sludge. Current practice does not make use of this resource; instead, P and K concentrations in the process water are limited, requiring supplementation for aquaponics (NPK-fertilizer) (Rennert et al. 2011). Additionally, the AT reduced NO₃⁻-N concentrations by just 16% compared to 97% in the unaerated treatment (UT), most probably due to denitrification. Thus, AT is a good compromise considering the overall supply of the nutrients for aquaponic applications.

Following AT, the phosphate concentration of 27.7 mg l⁻¹ PO₄³⁻ recorded here is still well below recommendations for industrial tomato production of around 160 mg l⁻¹ PO₄³⁻ (Hochmuth & Hochmuth

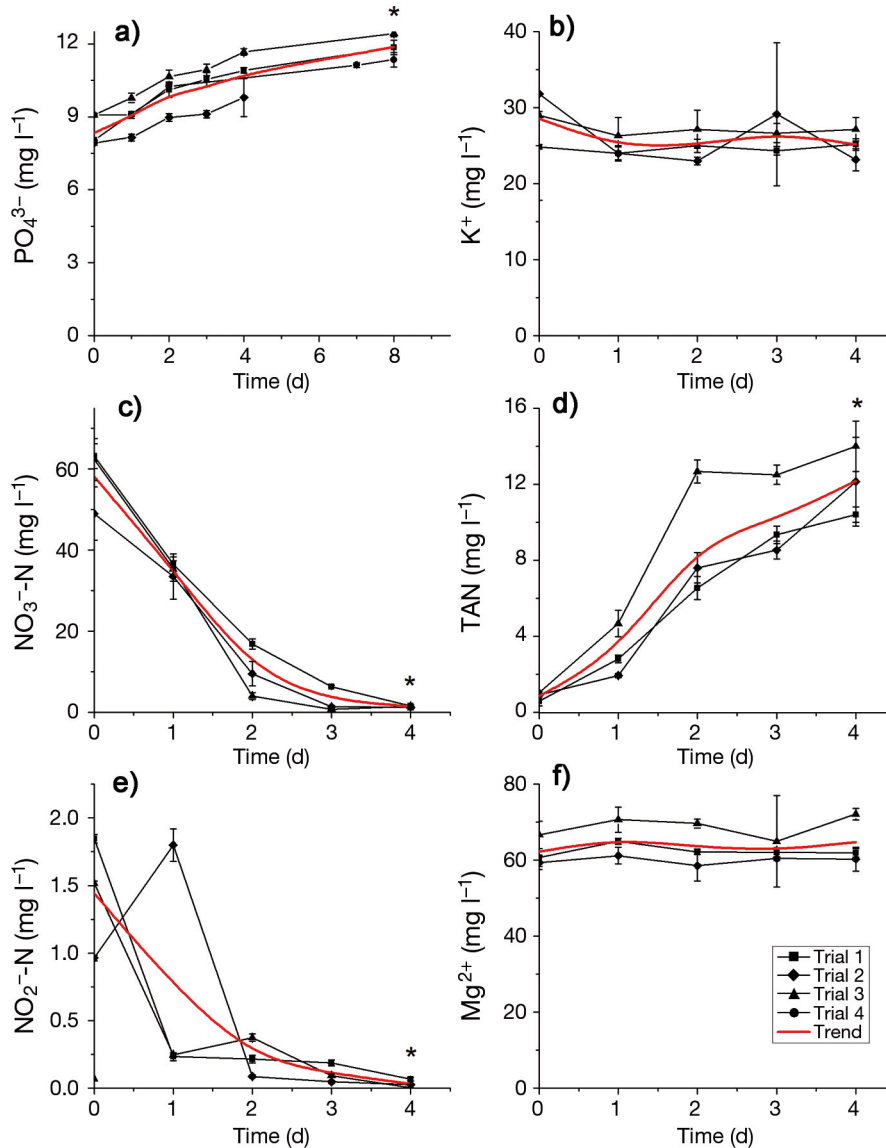


Fig. 2. Soluble nutrients (PO_4^{3-} , K^+ , total ammonia nitrogen [TAN], NO_3^- -N, NO_2^- -N, Mg^{2+}) in the liquid phase of a water-sludge mixture derived from a tilapia recirculating aquaculture system over 4 d (8 d only for soluble reactive phosphorus, PO_4^{3-}) of anaerobic mobilization (Expt 1). Data from 3 successive trials (4 trials for soluble reactive phosphorus PO_4^{3-}) are presented as mean \pm SD. Trend lines: means of the successive trials (technical replicates). *Significant differences compared to Day 0 are indicated by an asterisk ($p < 0.05$, Dunn's test, $n = 3$ or 4 trials).

2001). Our results are nonetheless very promising: a prolongation of incubation time as well as technological optimization would probably improve P mobilization further.

P is a key element for plant nutrition, essential for molecules such as ATP, nucleic acids and phospholipids (Schachtman et al. 1998). An optimal supply is thus essential to maximize plant growth. Recently, P use as fertilizer for agricultural production is subject of intense discussion in the scientific literature since estimations predict a depletion of this non-renewable resource (phosphate rock reserves, for

human fertilizer utilization) in coming decades (Cooper et al. 2011, McGill 2012); price surges have already been observed (McGill 2012). Currently, P for agricultural crop fertilization is mainly produced by mining (Schmid Neset et al. 2008) and sustainable recycling on a larger scale needs to be explored. Altogether, the increase of phosphate observed in this study particularly highlights the potential for an optimized nutrient recycling in aquaponic systems.

In contrast to AT, anaerobic treatment revealed only minor increases in SRP in the lab-scale experiments and even a slight decrease in the upscaling ex-

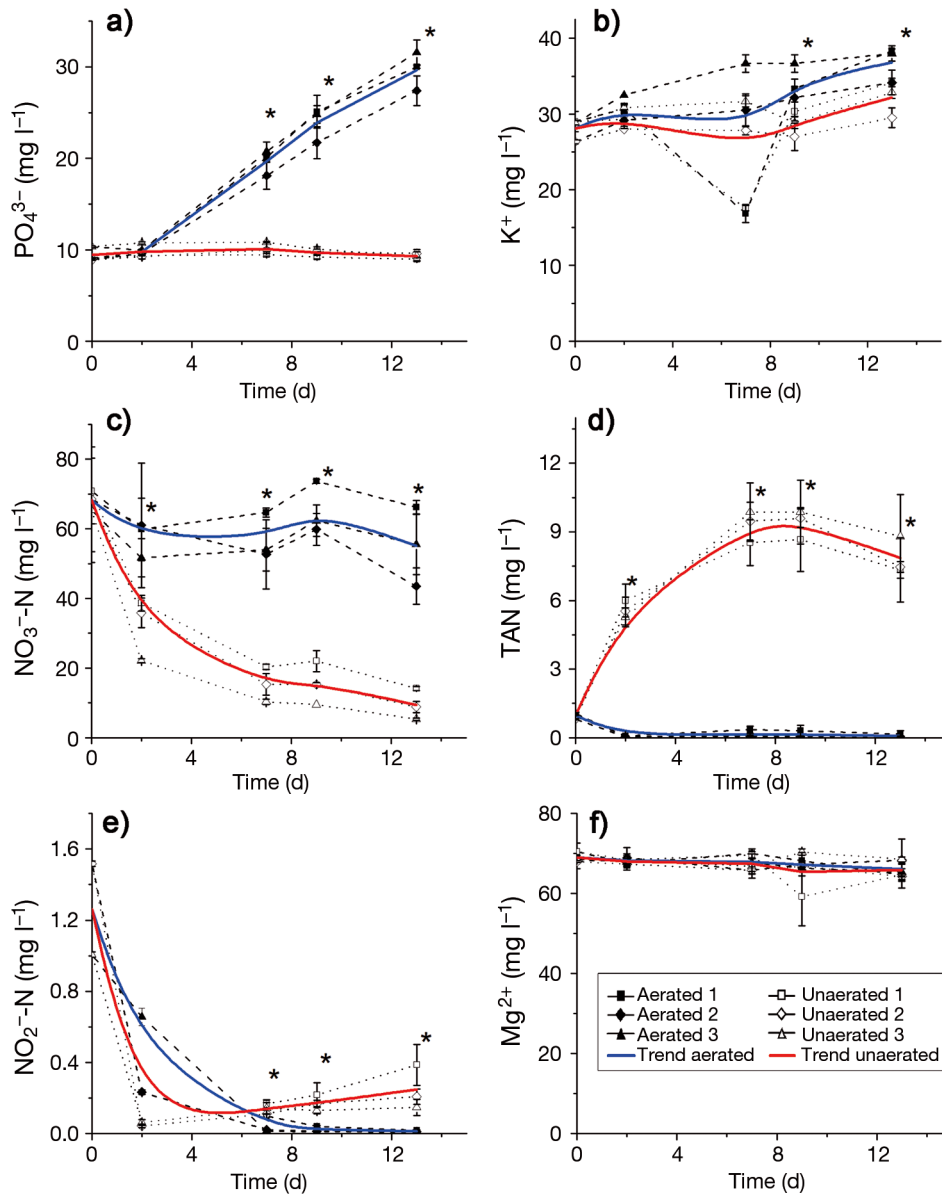


Fig. 3. Soluble nutrients (as in Fig. 2) in the liquid phase of a water-sludge mixture derived from a tilapia recirculating aquaculture system over 14 d (Day 0 to Day 13) of anaerobic (<0.1 mg O₂ l⁻¹, red) and aerobic (blue) treatment (Expt 2). Data from 3 successive trials per treatment are presented as means ± SD. Trend lines: mean of the successive trials. *Significant differences between anaerobic and aerobic mobilization (p < 0.05, Mann-Whitney U, n = 3 trials per treatment)

periments. Similarly, Jung & Lovitt (2011) reported a P-release of less than 5% within 7 d in anaerobic treatment of sludge from a trout farm. However, additional supplementation with glucose led to a final P-release of 90%. Interestingly, as suggested by those authors, glucose addition might not exhibit a direct effect on the P-release (e.g. by increase of P-solubilizing heterotrophs). Instead, lowering of the pH by glucose fermentation seemed to increase P leaching substantially (Jung & Lovitt 2011). In contrast to our study, a pH drop below 5 was observed after 24 h.

Furthermore, leaching of different nutrients including P was increased upon the addition of acids. Similarly, pH-dependent mobilization of P from fish sludge was also reported by Conroy & Couturier (2010). In our experiments, decreasing NO₃⁻-N indicated denitrification in all anaerobic treatments. Thus, proton consumption during denitrification (Klas et al. 2006) seemed to stabilize the pH in the anaerobic treatments, thereby reducing P (SRP) mobilization.

Accordingly, in the AT, continuous reduction in pH to 5.26 (± 0.01) over 14 d could mainly explain P

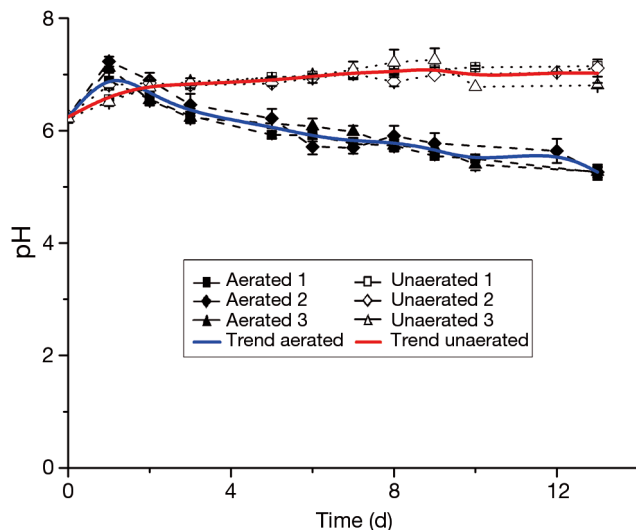


Fig. 4. pH in the liquid phase of a water-sludge mixture derived from a tilapia recirculating aquaculture system over 14 d (Day 0 to Day 13) of anaerobic ($<0.1 \text{ mg O}_2 \text{ l}^{-1}$, red) and aerobic (blue) mobilization. Data from 3 successive trials are presented as means \pm SD. Trend line: mean of the successive trials (technical replicates)

leaching in the present study. Here, both, nitrification processes as well as respiratory CO_2 production contribute to acidification in the incubator (Paredes et al. 2007, Wurts & Durborow 1992). An extended retention time and/or refilling with new sludge-water mixture or concentrated sludge could consequently speed up the pH decrease required and hence improve the mobilization.

During the study, we determined the P binding fractions in the sludge according to a modified sequential P fractionation scheme according to Hupfer et al. (1995) used in aquatic and soil science (Psenner et al. 1984). P fractionation results showed that 50% of TP were Ca-associated and thus pH sensitive. In the sequential P fractionation scheme this fraction is extracted with HCl and is determined as acid-soluble P fraction. Accordingly, when the pH decreases, a major part of the P in the fish sludge can be mobilized and become available for the crop plants. The second largest P-fraction (26%) in the sludge was loosely bound P (extracted with NH_4Cl) and is thus also easily mobilized. Finally, ~5% of the extracted P were associated with organic substances (poly-phosphates and humic substances; extracted with NaOH). Here, mobilization requires complex microbial digestion. An effective microflora established in the incubator may improve mobilization in the future, compared to the static approach assessed here. In our experiment, SRP increased by 20.2 mg l^{-1} and is estimated to represent a total of 30 g P mobilized from the sludge har-

vested from the clarifier (1.5 m^3) after 1 wk. The solid phase analyses of the fish sludge from the clarifier revealed TP values of $60 \text{ g harvest}^{-1}$. Thus, considering the fractionation analysis, this increase may only result from pH-labile P (50% of TP) in the fish sludge.

Compared to AT, anaerobic treatment is less efficient in the incubator used, but could be optimized by addition of acids, carbon sources and/or bacterial suspension. Undoubtedly, even after completion of the necessary research, an optimised anaerobic treatment process would still require further maintenance effort, resources and the reoxygenation of anaerobic water for subsequent hydroponic application. More important, nitrate, which constitutes the most important nutrient source derived from RAS, would be lost for aquaponic application. Here, an easy-to-handle approach was evaluated particularly with regard to the requirements in aquaculture practice and the need for cost-optimization in current aquaculture operations.

Undoubtedly, the choice of fish species and feed used is utmost relevant in this respect. Particularly for tilapia *Oreochromis niloticus*, due to economic feasibility, fishmeal is often fully substituted by plant ingredients (e.g. soybean meal, rape seed press cake and meal) without adverse effects on fish performance (El-Saidy & Gaber 2002). With regard to the current trend towards sustainable aquafeeds replacing fishmeal (Samuel-Fitwi et al. 2012, Slawski et al. 2012, Tusche et al. 2012, 2013) phytate is the main storage form for P in plant ingredients. Here, phosphate bioavailability is reduced, requiring enzymatic (phytase) conversion (Kumar et al. 2012). Thus, the use of animal protein derived from sustainable resources such as blood, insect or feather meal is a worthwhile strategy to optimize diets for aquaponics in the future. Alternatively, one could increase mobilization of plant-derived, organic P by optimizing enzymatic conversion either by using phytase supplementation in the fish diet (which would also increase P availability for the fish and thus improve fish nutrition) or by increasing microbial conversion. The latter will inevitably require a more sophisticated incubator that may not be feasible under the current economic and operational conditions.

The increase of K^+ by 31% is particularly relevant in tomato production since this macronutrient is required in large amounts and is currently only covered by artificial fertilization (Lattauschke 2004). Nevertheless, K^+ is not a scarce resource like P and the increase was not as significant as the increase in P. Still, optimized nutrient management in aquaponics should ultimately aim to minimize use of artificial

fertilizer. Also, to our knowledge, current legislation and fees for aquaculture emissions do not consider respective K^+ concentrations. Nevertheless, envisioning sustainable nutrient re-use, future studies should focus on an overall optimization strategy to ensure an environmentally friendly production cycle.

In this context, although not determined in our study, potential accumulation of sodium has to be considered since this is an important issue in hydroponics. Up to a point, excess NaCl in the nutrient solution can be excluded by the plants; however, in a recirculating system this will result in a steady increase in salt concentration (Blom-Zandstra et al. 1998). Therefore hydroponics nutrient solution is frequently renewed to avoid excessively high salt concentrations and thus to prevent reduction of fruit yield or increased sensitivity to diseases (Post & Klein-Buitendijk 1996a,b).

The reduction of NO_3^- -N by 19% is only relevant in critical periods, when imbalances between standing stock of fish and plant production cannot be avoided, for example upon harvest or in periods when fish growth varies unexpectedly (e.g. stress). In well-balanced aquaponic systems, the reduction could be of minor relevance since intensive RAS production supports high NO_3^- -N concentrations of up to 1000 mg l^{-1} in the rearing water, and blending with water from the sludge incubator can easily be compensated (van Rijn 2013). Under anaerobic conditions, loss of nitrogen due to denitrification was substantial and has to be taken into account for the overall evaluation of AT and UT studied here.

In the present study, TS was lower than in other studies. For example, Conroy & Couturier (2010) reported 109 g l^{-1} TS before initiating anaerobic treatment, i.e. 50 to 100 times higher than in the present study. This mostly results from differently concentrated sludge. Here, we prioritized a simple, easy-to-handle harvest of sludge. Still, both studies identified a P mobilization after a drastic drop in pH below 6. Consequently, it can be concluded that mobilization is—mainly—observed after acidification. Furthermore, higher TS may result in acidification due to massive fermentation under anaerobic conditions, whereas at lower TS acidification due to respiration at AT is demonstrated here. Together, this emphasizes the principal role of pH in sludge treatment. With respect to handling, system safety and reducing labour costs and providing a robust sludge treatment, aerobic treatment of water-sludge mixture can easily be integrated in aquaponic systems and, compared to anaerobic treatment, does not imply a loss of nitrogen by anaerobic denitrification.

CONCLUSIONS

In our study we comparatively evaluated a simple, easy-to-handle sludge incubation under aerobic and anaerobic treatment to improve the mobilization of important nutrients required for plant production. Here, aeration establishes aerobic conditions, and lowers the pH (via respiration and nitrification), subsequently supporting mobilization of P and K^+ with minor losses of NO_3^- -N. Thereby, the delivery of these nutrients for the crop plant production is clearly improved in the overall system, reducing nutrient emission from sludge disposal. In contrast, anaerobic conditions (e.g. as in denitrification units) revealed a complete loss of NO_3^- -N, poses the risk of undesired byproducts and, in practice, is more complicated to handle under commercial conditions. Based on our results we recommend a simple aeration (aerobic treatment) for the effective nutrient mobilization for aquaponics. Still it needs to be emphasized that economic feasibility and biological safety has to be proven. Also, application might be restricted to highly technical and complex systems.

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